

- 7-5. Using the sweep-through purging method, inert a 100 gallon vessel containing 100% air until the oxygen concentration is 1%. What volume of nitrogen is required? Assume nitrogen with no oxygen and a temperature of 77°F.

Eq 7-10 applied

$$Q_v t = V \ln \left( \frac{C_1 - C_0}{C_2 - C_0} \right)$$

$$C_1 = .21$$

$$C_0 = 0$$

$$C_2 = .01$$

$$Q_v t = (100 \text{ gal}) \left( \frac{\text{ft}^3}{7.48 \text{ gal}} \right) \ln \left[ \frac{.21 - 0}{.01 - 0} \right] = \underline{\underline{40.7 \text{ ft}^3}}$$

- 7-7. Use a vacuum purging technique to purge oxygen out of a 150 cubic ft tank containing air. Reduce the oxygen concentration to 1% using pure nitrogen as the inert. The temperature is 80°F. Assume the vacuum purge goes from atmospheric pressure to 20 mm Hg. absolute. Determine the number of purge cycles required, and the total moles of nitrogen used.

Relation 7-6

$$y_j = y_0 \left( \frac{P_L}{P_H} \right)^j = y_0 \left( \frac{n_L}{n_H} \right)^j \ln \left( \frac{y_j}{y_0} \right) = j \ln \left( \frac{P_L}{P_H} \right)$$

$$y_j = .01 \qquad j = \frac{\ln \left( \frac{y_j}{y_0} \right)}{\ln \left( \frac{P_L}{P_H} \right)}$$

$$y_0 = .21$$

$$P_L = 20 \text{ mmHg}$$

$$P_H = 760 \text{ mmHg}$$

$$j = \frac{\ln \left( \frac{.01}{.21} \right)}{\ln \left( \frac{20}{760} \right)} = \frac{-3.045}{-3.638} = 0.837$$

So use one purge cycle

Total moles  $N_2$  used - Eq 7-7

$$\Delta n_{N_2} = j (P_H - P_L) \frac{V}{R_g T} = (1) \frac{(760 \text{ mmHg} - 20 \text{ mmHg}) (150 \text{ ft}^3) \left( \frac{\text{atm}}{760 \text{ mmHg}} \right)}{\left( 0.7302 \frac{\text{ft}^3 \text{ atm}}{\text{lbmol} \cdot \text{R}} \right) (460 + 80 \text{ R})}$$

$$\Delta n_{N_2} = 0.370 \text{ lbmol } N_2$$

7-10. Use the system described in Figure 7-2 to determine the voltage developed between the charging nozzle and the grounded tank, and the energy stored in the nozzle. Explain the potential hazard for cases a and b below.

Case	a	b
Hose length (ft)	20	20
Hose diameter (in)	2	2
Flow rate (gpm)	25	25
Liquid conductivity (mho/cm)	$10^{-8}$	$10^{-18}$
Dielectric constant	2.4	19
Density (gm/cm <sup>3</sup> )	0.8	0.8
Viscosity (centipoise)	0.6	0.6
Diffusivity, $D_m$ (cm <sup>2</sup> /s)	$2.2 \times 10^{-5}$	$2.2 \times 10^{-5}$

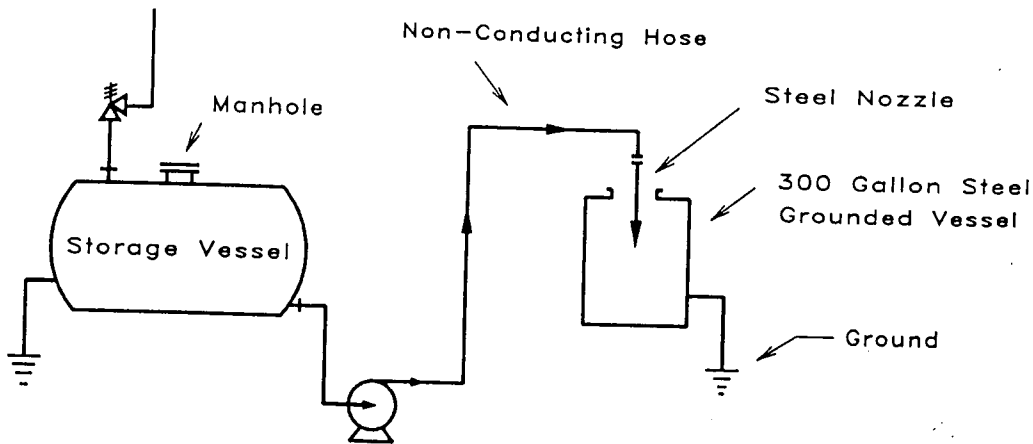


Figure 7-2

Since the nozzle & hose are not grounded, voltage generated at nozzle is  $V = IR$

Resistance calculated by (Eq 7-18)

$$R = \frac{L}{\gamma_c A}$$

Current, will be streaming current 7-12 or 7-14 depending (laminar or turbulent)

Find Reynolds number  $Re = \frac{d \bar{u} \rho}{\mu}$

$$R\bar{u} = \left(25 \frac{\text{gal}}{\text{min}}\right) \left(\frac{f^3}{7.481 \text{ gal}}\right) \left(\frac{\text{min}}{60 \text{ s}}\right) \left(\frac{1}{\pi}\right) \left(\frac{1}{1 \text{ in.}}\right)^2 \left(\frac{12 \text{ in.}}{\text{ft}}\right)^2 = 2.553 \text{ ft/s}$$

$$Re = \frac{d \bar{u} \rho}{\mu} = \frac{(2 \text{ in.}) (2.553 \text{ ft/s}) (.8 \text{ g/cm}^3)}{(0.6 \text{ centipoise})}$$

$$= 6.808 \frac{\text{in} \cdot \text{ft}}{\text{s} \cdot \text{cm}^3} \times \left(\frac{12 \text{ in.}}{1 \text{ ft}}\right) \left(\frac{2.54 \text{ cm}}{1 \text{ in.}}\right)^2 \left(\frac{100 \text{ cP}}{\text{Poise}}\right) \left(\frac{\text{Poise}}{0.1 \text{ g/cm} \cdot \text{s}}\right)$$

$$\times \frac{1 \text{ ft}}{1000 \text{ g}} \times \frac{100 \text{ cm}}{\text{m}} = \underline{52,707} \text{ turbulent}$$

Eq 7-14 applies

$$I_s = \left[ \frac{5.89 \times 10^{-14} \text{ amp}}{(\text{ft/s}) (\text{volt})} \right] \frac{d \epsilon_r \zeta \bar{u}}{\delta}$$

$\zeta$  = zeta potential 0.01 to 0.1

use 0.1 as worst case

$\delta$  = double layer thickness - given by Eq 7-15

$$\delta = \sqrt{Dm\tau}$$

$\tau$  = relaxation time given by Eq 7-16

$$\tau = \frac{\epsilon_r \epsilon_0}{\gamma_c}$$

$$\tau = \frac{(2.4)(8.85 \times 10^{-12} \frac{\text{Coulomb}^2}{\text{J}\cdot\text{m}})}{(10^{-8} \text{ mho/cm})} \cdot \left(\frac{\text{m}}{100\text{cm}}\right) \cdot \left(\frac{\text{J/Volt}}{\text{Coulomb}}\right) \left(\frac{\text{Amp}\cdot\text{s}}{\text{Coulomb}}\right) \left(\frac{\text{mho}}{\text{amp/V}}\right)$$

$$\tau = 2.12 \times 10^{-5} \text{ sec}$$

$$\delta = \sqrt{Dm\tau} = \sqrt{(2.2 \times 10^{-5} \frac{\text{cm}^2}{\text{s}})(2.12 \times 10^{-5} \text{ s})}$$

$$\delta = 2.162 \times 10^{-5} \text{ cm}$$

$$I_s = \left[ \frac{5.89 \times 10^{-14} \text{ amps}}{(\text{A/s})(\text{Volt})} \right] \frac{(2 \text{ in.})(2.4)(0.1 \text{ Volt})(2.553 \text{ ft/s})}{(2.162 \times 10^{-5} \text{ cm})} \left( \frac{2.54 \text{ cm}}{\text{in.}} \right)$$

$$I_s = 8.48 \times 10^{-9} \text{ amps}$$

$$R = \frac{L}{\gamma_c A} = \frac{20 \text{ ft}}{(10^{-8} \text{ mho/cm}) (\pi (1 \text{ in.})^2) \left( \frac{12 \text{ in.}}{\text{ft}} \right) \left( \frac{1 \text{ in.}}{2.54 \text{ cm}} \right)}$$

$$R = 3.008 \times 10^9 \text{ ohm}$$

$$V = I_s R = (8.48 \times 10^{-9} \text{ amps})(3.008 \times 10^9 \text{ ohm}) = \boxed{25.5 \text{ volts}}$$

To calculate accumulated charge, Eg 7-22

$$Q = I s t$$

Time to fill tank

$$\left( \frac{300 \text{ gallon}}{25 \text{ gallon/min}} \right) \left( \frac{60 \text{ s}}{\text{min}} \right) = \underline{720 \text{ seconds}}$$

$$Q = (8.48 \times 10^{-9} \text{ amps}) (720 \text{ seconds}) = \underline{6.106 \times 10^{-6} \text{ coulombs}}$$

Calculate capacitance

$$C = Q/V = \frac{6.106 \times 10^{-6} \text{ coulombs}}{25.5 \text{ volts}} = \underline{2.394 \times 10^{-7} \text{ Farads}}$$

Calculate accumulated energy

$$J = \frac{Q^2}{2C} = \frac{(6.106 \times 10^{-6})^2}{2(2.394 \times 10^{-7})} = \boxed{7.786 \times 10^{-5} \text{ J}}$$

0.078 mJ

This is below MIE - no problem, but safest to have the system bonded and grounded.

- (b) Repeat - only changes  $\epsilon_r = 19$ ,  $\gamma_c = 10^{-18}$   
Hence, fluid more of an insulator, less conductive

No change in Reynolds number

Relaxation time will change

$$\tau = \frac{\epsilon_r \epsilon_0}{\gamma_c} = \frac{(19)(8.85 \times 10^{-12} \text{ coulomb}^2/\text{J}\cdot\text{m})}{(10^{-18} \text{ mho/cm})} \left(\frac{\text{m}}{100\text{cm}}\right) \left(\frac{\text{J/Volt}}{\text{coulomb}}\right) \left(\frac{\text{Amps}}{\text{Coul}}\right) \left(\frac{\text{mho}}{\text{amp/V}}\right)$$

$$\tau = \underline{1.6815 \times 10^6 \text{ sec}}$$

Determine double layer thickness

$$\delta = \sqrt{D_m \tau} = \sqrt{(2.2 \times 10^{-5} \text{ cm}^2/\text{s})(1.6815 \times 10^6 \text{ sec})} = \underline{6.082 \text{ cm}}$$

Determine streaming current

$$I_s = \left[ \frac{5.89 \times 10^{-14} \text{ amp}}{(\text{ft/s})(\text{volt})} \right] \frac{d \epsilon_r \zeta \bar{u}}{\delta}$$

$$I_s = \frac{5.89 \times 10^{-14} \text{ amp}}{(\text{ft/s})(\text{volt})} \frac{(2 \text{ in.})(19)(.1 \text{ volt})(2.553 \text{ ft/s})}{6.082 \text{ cm}} \left(\frac{2.54 \text{ cm}}{\text{in.}}\right) = \underline{2.386 \times 10^{-13} \text{ amp}}$$

Calculate resistance

$$R = \frac{L}{\gamma_c A} = \frac{20 \text{ ft}}{(10^{-18} \text{ mho/cm})(\pi)(1 \text{ in.})^2} \left(\frac{12 \text{ in.}}{\text{ft}}\right) \left(\frac{1 \text{ in.}}{2.54 \text{ cm}}\right) = 3.008 \times 10^{19} \text{ ohm}$$

Calculate Voltage

$$V = I_s R = (2.386 \times 10^{-13} \text{ amp}) (3.008 \times 10^{19} \text{ ohm}) = \underline{\underline{7.177 \times 10^6 \text{ volt}}}$$

Calculate Accumulated charge Eq 7-22

$$Q = I_s t$$

$$Q = (2.386 \times 10^{-13} \text{ amp}) (720 \text{ s}) = 1.718 \times 10^{-10} \text{ coulomb}$$

Calculate Capacitance

$$C = Q/V = \frac{1.718 \times 10^{-10} \text{ coulombs}}{7.177 \times 10^6 \text{ volts}} = 2.394 \times 10^{-17} \text{ farads}$$

Calculate accumulated energy

$$J = \frac{Q^2}{2C} = \frac{(1.718 \times 10^{-10})^2}{2(2.394 \times 10^{-17})} = 0.00617 \text{ J}$$

$$= \underline{\underline{0.617 \text{ mJ}}}$$

The voltage and energy are high enough to cause a spark which will explode.

Need to bond & ground nozzle.