## FLOW METER PIPING REQUIREMENTS

"Diameters" of straight pipe required for various types of flow meters

Diameter (D) = nominal Pipe Size
Example:
13 Diameters of 6" pipe $=78^{\prime \prime}$
13 Diameters of 10 " pipe $=130 "$
Beta $=($ Bore I.D./Pipe I.D. $)$ Bore is the smallest diameter of an orifice or nozzle

Up = Upstream Diameters Down = Downstream Diameters

| Orifice/Nozzle | Beta $=0.5$ | Up | 6 | 11 | 26 |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Down | 3 | 3 | 3 |
|  | Beta $=0.7$ | Up | 10 | 15 | 38 |
|  |  | Down | 4 | 4 | 4 |
| Venturi | Beta $=0.5$ | Up | 5 | 7 | 7 |
|  |  | Down | 2 | 2 | 2 |
|  | Beta $=0.7$ | Up | 9 | 26 | 26 |
|  |  | Down | 4 | 4 | 4 |
| Vortex |  | Up | 25 | 25 | 30 |
|  |  | Down | 5 | 5 | 5 |
| Thermal |  | Up | 15 | 15 | 40 |
|  |  | Down | 5 | 5 | 5 |
| Turbine |  | Up | 10 | 10 | 10 |
|  |  | Down | 5 | 5 | 5 |
| Annubar |  | Up | 8 | 9 | 24 |
|  |  | Down | 3 | 3 | 4 |

## Note:

1. The straight runs shown above are conservative minimums. Longer upstream straight pipe lengths provide better accuracy.
2. If the indicated straight run is not available, Consult Factory. Detailed Factory analysis will require accurate fluid data, flow data, and a sketch detailing the piping system 50 diameters upstream and 10 diameters downstream from the proposed meter location.
3. Internal straightening vanes can be used to reduce straight pipe length requirements, Consult Factory.
4. Positive Displacement and Coriolis Effect Meters are not influenced by upstream and downstream fittings.

## FLOW METER PIPING REQUIREMENTS

## "Diameters" of straight pipe required for various types of flow meters

| Diameter ( D ) = nominal Pipe Size |  |  | Two Elbows, > 10 Diameters, Fittings in Different Planes | Two Elbows, < 10 Diameters, Fittings in Different Planes | $\begin{aligned} & \text { Reducer or Expander } \\ & \text { (Unless Another } \\ & \text { Upstream fitting Needs More) } \end{aligned}$ | Atmospheric Intake |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 13 Diam 13 Diam <br> Beta <br> Bore is the sm <br> Up $=$ <br> Down = | xample: <br> rs of 6" pipe s of 10" pipe <br> ore I.D./Pipe est diameter r nozzle <br> tream Diam nstream Dia | " <br> orifice |  |  |  |  |
| Orifice/Nozzle | Beta $=0.5$ | Up | 16 | 20 | 9 | 8 |
|  |  | Down | 3 | 3 | 3 | 3 |
|  | Beta $=0.7$ | Up | 23 | 30 | 12 | 9 |
|  |  | Down | 4 | 4 | 4 | 4 |
| Venturi | Beta $=0.5$ | Up | 21 | 21 | 5 (reducer), 2 (expander) | - |
|  |  | Down | 2 | 2 | 2 | - |
|  | Beta $=0.7$ | Up | 21 | 21 | 8 (reducer), 4 (expander) | - |
|  |  | Down | 2 | 2 | 4 | - |
| Vortex |  | Up | 30 | 45 | 25 | - |
|  |  | Down | 5 | 5 | 5 | - |
| Thermal |  | Up | 15 | 40 | 15 (reducer), 30 (expander) | - |
|  |  | Down | 5 | 10 | 5 (reducer), 10 (expander) | - |
| Turbine |  | Up | 10 | 10 | 10 | - |
|  |  | Down | 5 | 5 | 5 | - |
| Annubar |  | Up | 9 | 19 | 8 | - |
|  |  | Down | 3 | 4 | 3 | - |

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Bore is the smallest diameter of an orifice or nozzle

Up $=$ Upstream Diameters
Down $=$ Downstream Diameters

## Note:

One Elbow, T, Y, or Tank Exit (Fittings in the Same Plane)


| Orifice/Nozzle | Beta $=0.5$ | Up | 7 |
| :---: | :---: | :---: | :---: |
|  |  | Down | 3 |
|  | Beta $=0.7$ | Up | 13 |
|  |  | Down | 4 |
| Venturi | Beta $=0.5$ | Up | 4 |
|  |  | Down | 2 |
|  | Beta $=0.7$ | Up | 4 |
|  |  | Down | 2 |
| Vortex |  | Up | 30 |
|  |  | Down | 5 |
| Thermal |  | Up | 15 |
|  |  | Down | 5 |
| Turbine |  | Up | 10 |
|  |  | Down | 5 |
| Annubar |  | Up | 7 |
|  |  | Down | 3 |

Two Elbows (Fittings in the Same Plane)

| 10 |  |
| :---: | :---: |
| (For Two Elbows >10D separation, |  |
| use One Elbow Data) |  |

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